

Listing of the Claims:

This listing of the claims will replace all prior versions and listings of claims in the application.

1. (Currently Amended) A sulfate process for producing titania from a titaniferous material which includes the steps of:
 - (a) leaching the titaniferous material with a leach solution containing sulfuric acid and forming a leach liquor that includes an acidic solution of titanyl sulfate (TiOSO_4) and iron sulfate (FeSO_4);
 - (b) separating the leach liquor and a residual solid phase from the leach step (a);
 - (c) separating titanyl sulfate from the leach liquor from step (b) and using at least part of the leach liquor that remains after separation of the titanyl ~~sulfate~~ sulfate as part of the leach solution in one of the leach step (a) or a further leach step;
 - (d) hydrolysing the separated titanyl sulfate and forming a selected particle size distribution of hydrated titanium oxides from titanyl sulfate;
 - (e) separating the hydrated titanium oxides from a liquid phase that ~~are~~ is produced in the hydrolysis step (d); and
 - (f) calcining the solid phase from step (e) and forming titania.
2. (Previously Presented) The process defined in claim 1 further comprising controlling the hydrolysis step (d) to produce a selected particle size distribution of the hydrated titanium oxides product.
3. (Currently Amended) The process defined in claim 1 further comprising controlling the hydrolysis step (d) to produce coarse hydrated titanium oxides, ~~i.e.~~ oxides having a particle size of at least 0.005 mm.
4. (Currently Amended) The process defined in claim 1 further comprising controlling the hydrolysis step (d) to produce fine hydrated titanium oxides, ~~i.e.~~ oxides having a particle size of less than 0.0003 mm.

5. (Previously Presented) The process defined in claim 1 further comprising a further leach step of leaching the residual solid phase from step (b) with a leach solution containing sulfuric acid and forming a leach liquor that includes an acidic solution of titanyl sulfate and iron sulfate and a residual solid phase.
6. (Original) The process defined in claim 5 wherein the further leach step includes separating the leach liquor and the residual solid phase.
7. (Original) The process defined in claim 5 wherein the further leach step includes supplying the separated leach liquor to the leach step (a) and/or mixing the separated leach liquor with the leach liquor from step (b).
8. (Previously Presented) The process defined in claim 5 further comprising carrying out the leach step (a) and the further leach step in the same vessel.
9. (Previously Presented) The process defined in claim 8 further comprising returning the residual solid phase from step (b) to the vessel, wherein the residual solid phase forms part of the titaniferous material subjected to leaching in the leach step (a).
10. (Previously Presented) The process defined in claim 5 further comprising carrying out the leach step (a) and the further leach step in a separate vessel or vessels.
11. (Original) The process defined in claim 10 wherein the further leach step includes supplying the residual solid phase from step (b) to the vessel or vessels.
12. (Previously Presented) The process defined in claim 5 wherein the leach step (a) and/or the further leach step includes selecting and/or controlling the leach conditions in the leach step or steps to avoid undesirable amounts of premature

hydrolysis of hydrated titanium oxides and undesirable amounts of premature precipitation of titanyl sulfate.

13. (Original) The process defined in claim 12 wherein the leach conditions include any one or more than one of acid concentration, leach temperature and leach time.

14. (Previously Presented) The process defined in claim 12 further comprising selecting and/or controlling the acid concentration to be at least 350 g/l sulfuric acid throughout the leach step (a) and/or the further leach step when operating at a leach temperature in the range of 95°C to the boiling point in order to avoid premature hydrolysis.

15. (Previously Presented) The process defined in claim 12 further comprising selecting and/or controlling the acid concentration at the end of the leach step (a) and/or the further leach step to be less than 450 g/l when operating at a leach temperature in the range of 95°C to the boiling point in order to avoid an undesirable amount of premature precipitation of titanyl sulfate.

16. (Previously Presented) The process defined in claim 12 further comprising selecting and/or controlling the leach conditions so that the titanium ion concentration in the leach liquor is less than 50 g/l in the leach liquor at the end of the leach step (a) and/or the further leach step.

17. (Previously Presented) The process defined in claim 16 further comprising selecting and/or controlling the leach conditions so that the titanium ion concentration in the leach liquor is 40-50 g/l in the leach liquor at the end of the leach step (a) and/or the further leach step.

18. (Previously Presented) The process defined in claim 5 further comprising carrying out the leach step (a) and/or the further leach step in the presence of a leaching accelerant that accelerates the rate of leaching the titaniferous material.

19. (Previously Presented) The process defined in claim 18 wherein the leaching accelerant is selected from the group consisting of iron, a titanium (III) salt, a thiosulfate salt, sulfur dioxide, a reduced sulfur containing species, and mixtures thereof.

20. (Previously Presented) The process defined in claim 5 further comprising carrying out the leach step (a) and/or the further leach step in the presence of a reductant that reduces ferric ions to ferrous ions in the acidic solution or solutions of titanyl sulfate and iron sulfate produced in the leach step (a).

21. (Previously Presented) The process defined in claim 20 wherein the reductant is selected from the group consisting of iron, a titanium (III) salt, a thiosulfate salt, sulfur dioxide, a reduced sulfur containing species, and mixtures thereof.

22. (Previously Presented) The process defined in claim 1 further comprising the steps of precipitating iron sulfate from the leach liquor from step (b) and separating precipitated iron sulfate from the leach liquor prior to the titanyl sulfate separation step (c).

23. (Canceled)

24. (Previously Presented) The process defined in claim 1 wherein the titanyl sulfate separation step (c) includes a solvent extraction step of extracting titanyl sulfate from the leach liquor from step (b) into a solvent and thereafter stripping titanyl sulfate from the solvent and forming a solution that contains titanyl sulfate and thereafter hydrolysing the titanyl sulfate-containing solution in the hydrolysis step (c).

25. (Previously Presented) The process defined in claim 24 further comprising using at least part of a raffinate from the solvent extraction step as at least part of the leach solution in leach step (a) and/or in the further leach step.
26. (Original) The process defined in claim 25 wherein the leach solution in the leach step (a) and the further leach step includes the raffinate and make-up fresh sulfuric acid.
27. (Previously Presented) The process defined in claim 25 wherein the raffinate from the solvent extraction step has an acid concentration of at least 250 g/l sulfuric acid.
28. (Previously Presented) The process defined in claim 24 wherein the solvent extraction step includes contacting the leach liquor with the solvent and a modifier.
29. (Cancelled)